

(12)

EUROPEAN PATENT APPLICATION

(21) Application number: 84305676.3

(51) Int. Cl.⁴: C 10 G 11/18

(22) Date of filing: 21.08.84

(30) Priority: 06.09.83 US 529824

(43) Date of publication of application:
02.05.85 Bulletin 85/18

(84) Designated Contracting States:
BE DE FR GB IT NL

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(64) Closed reactor FCC system with provisions for surge capacity.

(67) The present invention involves a fluid catalytic cracking (FCC) apparatus and process comprising a reactor riser zone, a primary and a secondary cyclones, connected in series to the riser zone, and a stripping zone. The riser zone, the primary and the secondary cyclones, and the stripping zone, are placed within a single reactor vessel. The primary cyclone is connected to the reactor riser zone by an enclosed conduit which prevents random post-riser thermal cracking of the hydrocarbons after they exit the reactor riser zone. The conduit contains a trickle valve, or other means, to accommodate sudden increased surges of flow of the hydrocarbons and catalyst mixture.

EP 0 139 392 A1

CLOSED REACTOR FCC SYSTEM WITH PROVISIONS FOR SURGE CAPACITY

This invention relates to the separation of the catalyst phase from the gasiform phase in a fluidized catalytic cracking unit (FCC) reactor. More particularly, it relates to improvements in separating the catalyst phase from the gasiform phase, as the suspension comprising both phases is discharged from a riser conversion, i.e. riser cracking, zone outlet, to minimize or substantially eliminate post-riser conversion zone cracking.

The field of catalytic cracking, particularly fluid catalytic cracking, has undergone significant development improvements due primarily to advances in catalyst technology and product distribution obtained therefrom. With the advent of high activity catalysts and particularly crystalline zeolite cracking catalysts, new areas of operating technology have been encountered requiring even further refinements in processing techniques to take advantage of the high catalyst activity, selectivity and operating sensitivity.

Of particular concern in this field has been the development of methods and systems for separating gasiform products from fluidizable catalyst particles, particularly from a high activity crystalline zeolite cracking catalysts, under more efficient separating conditions so as to reduce the overcracking of conversion products and promote the recovery of desired products of a hydrocarbon conversion operation. However, present day cyclonic equipment often permits an undesired extended residence time of the product vapor within a large reactor vessel. This extended residence time causes a loss of the desired product yield of up to about 4 percent through non-selective thermal cracking. Recent developments in this art have been concerned with the rapid separation and recovery of entrained catalyst particles from gasiform products in a short contact time riser hydrocarbon conversion operation.

The hydrocarbon conversion catalyst usually employed in an FCC installation is preferably a high activity crystalline zeolite catalyst of a fluidizable particle size which is transferred in suspended or

dispersed phase condition generally upwardly through one or more riser conversion zones providing a hydrocarbon residence time in each conversion zone in the range of 0.5 to about 10 seconds, and more usually less than about 8 seconds. High temperature riser hydrocarbon conversions of at least 1000°F (538°C) at 0.5 to 4 seconds hydrocarbon residence time in contact with the catalyst in the riser are desirable for some operations before initiating separation of vaporous hydrocarbon product materials from the catalyst. Rapid separation of catalyst from hydrocarbons discharged from a riser conversion zone is particularly desirable for restricting hydrocarbon conversion time. During the hydrocarbon conversion step, carbonaceous deposits accumulate on the catalyst particles and the particles entrain hydrocarbon vapors upon removal from the catalyst conversion step. The entrained hydrocarbons are subjected to further contact with the catalyst until they are removed from the catalyst by mechanical means and/or stripping gas in a separate catalyst stripping zone. Hydrocarbon conversion products separated from the catalyst and stripped materials are combined and passed to a product fractionation step. Stripped catalyst containing deactivating amounts of carbonaceous material, hereinafter referred to as coke, is then passed to a catalyst regeneration operation.

Various processes and mechanical means have been employed heretofore to effect rapid separation of the catalyst phase from the hydrocarbon phase at the termination of the riser cracking zone, to minimize contact time of the catalyst with cracked hydrocarbons.

Cartmell, U. S. Patent 3,661,799, discloses a process for catalytic conversion of petroleum feedstocks wherein the fluidized mixture of the cracking catalyst and cracked feedstock leaves a vertically-disposed reactor section and enters a cyclone separator, placed in a separate stripper vessel, through a conduit. The conduit contains an annulus which allows an inert stripping gas and associated stripped vapors to pass into the cyclone separator.

Anderson, et al., U. S. Patent 4,043,899, disclose a method for rapid separation of a product suspension comprising fluidized catalyst particles and the vaporous hydrocarbon product phase by discharging the entire suspension directly from the riser conversion zone into a cyclonic

separation zone which provides cyclonic stripping of the catalyst after it is separated from the hydrocarbon vapors. In the method of Anderson et al., the cyclone separator is modified to include an additional downwardly extending section comprising a lower cyclone stage. In this arrangement, catalyst separated from the gasiform material in the upper stage slides along a downwardly sloping baffle to the lower cyclone where stripping steam is introduced to further separate entrained hydrocarbon products from the catalyst recovered from the upper cyclone. The steam and the stripped hydrocarbons are passed from the lower cyclone through a concentric pipe where they are combined with the hydrocarbon vapors separated in the upper cyclone. The separated and stripped catalyst is collected and passes from the cyclone separator by conventional means through a dipleg. This process requires that the entire volume of catalyst, gasiform phase and stripping steam pass through the cyclone separator, which means that this equipment must be designed to efficiently handle not only a large vapor volume but also a large quantity of solid particles.

Myers et al., U. S. Patent 4,070,159, provide a separation means whereby the bulk of the solids is discharged directly into the settling chamber without passing through a cyclone separator. In this apparatus, the discharge end of the riser conversion zone is in open communication with the disengaging chamber such that the catalyst discharges from the riser in a vertical direction into the disengaging chamber which is otherwise essentially closed to the flow of gases. The cyclone separation system is in open communication with the riser conversion zone by means of a port located upstream from but near the discharge end of the riser conversion zone. A deflector cone mounted directly above the terminus of the riser causes the catalyst to be directed in a downward path so as to prevent the catalyst from abrading the upper end of the disengaging vessel. The cyclone separator is of the usual configuration employed in a catalytic cracking unit to separate entrained catalyst particles from the cracked hydrocarbon products so that the catalyst passes through the dipleg of the cyclone to the body of the catalyst in the lower section of the disengaging vessel and the vaporous phase is directed from this vessel to a conventional fractionation unit. There is

essentially no net flow of gases within the disengaging vessel beyond that resulting from a moderate amount of steam introduced to strip the catalyst residing in the bottom of the disengaging vessel.

Haddad et al., U. S. Patent 4,219,407, the entire contents of which are incorporated herein by reference, disclose the separation of the catalyst from the gasiform cracked products in a fashion which permits effective steam stripping of the catalyst. The suspension of catalyst and gasiform material is discharged from the riser conversion zone outwardly through radially extending passageways, or arms, which terminate in a downward direction. Catalyst stripping zones, or strippers, are located beneath the terminus of each of the radially extending passageways. Each stripper consists of a vertical chamber open at the top and the bottom with downwardly sloping baffles located within the chamber so as to cause the catalyst to flow in a circuitous manner countercurrently to upwardly flowing stripping steam introduced at the lower end of the stripping chamber. The radially extending arms are each provided with a curved inner surface and confining sidewalls to impart a cyclonic concentration of catalyst particles promoting a forced separation thereof from the hydrocarbon vapors. The separation of the catalyst from the vapors is basically achieved through rapid changes in the direction of flow of the catalyst and the vapors. Thus the cyclonic collection and concentration of catalyst particles is used to reverse the flow of separated catalyst such that it is concentrated as a downwardly confined stream which discharges generally downwardly and into the open upper end of the catalyst stripping chamber. A vapor disengaging space is provided between the discharge end of the radially extending arms and the top of the catalyst strippers to promote the rapid removal of separated vapors from the catalyst. The separated vapors pass upwardly through the disengaging vessel to the open inlet of a cyclone separator which removes entrained catalyst from the gasiform material for return through a dipleg to the body of steam stripped catalyst while the separated vaporous material passes to a fractionation unit. The hydrocarbon product, as it passes within the disengaging vessel from the discharge of the radially extending arms to the cyclone separator, travels in a random fashion and is exposed to catalytic reaction

temperatures which may cause undesirable side reactions and thermal cracking before these vapors enter a quench zone in the main fractionator of the fluid cracking unit.

Haddad et al., U.S. Patent No. 4,404,095, disclose an FCC reactor comprising a riser with radially extending sidearms as the first catalyst-hydrocarbon separation means. The sidearms force the suspension of the catalyst and the hydrocarbons to suddenly change the direction of flow from the vertical to the horizontal thereby forcing preliminary separation of the gaseous hydrocarbons from the solid catalyst particles. The catalyst particles fall in a downward direction, to a stripping means, while the hydrocarbons, with some entrained catalyst particles, proceed to a secondary separation means, such as a cyclone. The sidearms and the secondary separation means are enclosed by a vertical conduit to prevent random uncontrolled thermal cracking of the hydrocarbons. However, no means are provided in the apparatus and process of this Haddad et al. patent application for accommodating a sudden increase in pressure and the accompanying sudden increased rate of flow of the catalyst. Such unexpected increased pressure and the rate of flow of the cracking catalyst may be caused, for example, by mechanical malfunctions of equipment or by the vaporization of liquid water which may be introduced into the riser bottom with the hydrocarbon feed, or by unit pressure upsets.

It is a primary object of this invention to provide an improved process and apparatus for rapidly separating cracking catalyst from gasiform material and to provide an effective means of improving the ability of the FCC system to tolerate sudden system pressure increases and the accompanying surges in the catalyst rate of flow.

It is another object of this invention to provide an improved means for separating cracking catalyst from gasiform material in a fluid catalytic cracking (FCC) process.

It is a further object of this invention to provide a process and an apparatus for separating cracking catalyst from gasiform material whereby the length of time the gasiform material is subjected to high temperature after separation from the bulk of the catalyst is minimized so as to reduce non-selective thermal cracking of the vapor products.

These objectives can be realized in an improved FCC process and apparatus comprising a closed cyclone system for separating the catalyst from cracked hydrocarbon feed after the mixture of catalyst and feed exits the FCC cracking zone, e.g., the FCC riser. The system can be equipped with a means for providing a surge capacity to accommodate a sudden increased rate of flow of the catalyst stream. The closed cyclone system of the present invention comprises a primary cyclone means and a secondary cyclone means, or primary and secondary cyclones. The primary cyclone is connected to the FCC cracking zone by an enclosed conduit. The secondary cyclone is placed in-series with the primary cyclone, and the outlet of the primary cyclone is also connected by an enclosed conduit with the inlet of the secondary cyclone. The enclosed conduits limit the exposure of the cracked hydrocarbons to the high temperatures of the FCC reactor, thereby expediting the transfer of cracked hydrocarbons to the secondary cyclone means and preventing undesirable post-riser thermal cracking of the hydrocarbons. The solid catalyst particles are separated as a catalyst stream from the hydrocarbon vapors in the two cyclone separation means. Most of the catalyst stream from the cyclones is then directed to a disengaging zone, e.g., a steam stripper, placed below the cyclones, and the hydrocarbon product is directed to a downstream fractionation means. In accordance with the present invention, surge capacity means is provided in the enclosed conduit connecting the riser with the primary cyclone, in the enclosed conduit connecting the primary with the secondary cyclone, or in both. These enclosed conduits connect the riser with the primary cyclone and the primary with the secondary cyclones.

The process and apparatus of this invention can be illustrated by the drawings which are described in greater detail hereinafter.

Figure 1 is a schematic representation of a side view of a fluid catalytic cracking (FCC) reactor of the present invention.

Figure 2 is the front view of the FCC reactor of the present invention, taken along the axis A-A of Figure 1.

The means for providing surge capacity to accommodate the sudden increased pressure and the sudden increased rate of flow of the catalyst stream can be, for example, a trickle valve which is positioned in one or

both of the aforementioned enclosed conduits (e.g., see Figure 1). The trickle valve, or any other surge capacity means, is usually held closed by the higher pressure outside of the enclosed conduit than on the inside thereof. However, during the upset or surge conditions, the pressure inside the conduit exceeds that on the outside thereof forcing the surge capacity means to open and vent the excess material into the large reactor vessel surrounding the cyclones and the enclosed conduit. Therefore, in the event of a sudden unexpected surge of increased pressure and of the increased catalyst volume flow, the surge capacity means allows excess catalyst and hydrocarbon gases to exit the conduit, and the excess catalyst is deposited in the bottom of the reactor vessel. The provision of the surge capacity means prevents the primary and secondary cyclone dipleg flooding and large catalyst carryover from the FCC reactor to the main fractionation column, both of which might occur without the surge capacity means in the event of the surge conditions. In this connection, the term increased rate of catalyst flow, as used herein and in the appended claims, designates a short term 2 to 20-fold increase of catalyst flow by volume per unit of time of the steady state rate of flow of the catalyst stream. Similarly, the term sudden increase in pressure designates the pressure increase inside the enclosed conduit of 2-10 psi (28-70 kPa), as compared to the steady state operating conditions. In a conduit connecting the riser of the FCC reactor and the primary cyclone, there is provided a means, e.g., a slotted opening, to provide an opportunity for the major portion of the stripping steam and stripped hydrocarbon mixtures to enter the inside of the conduit and therefore of the primary and secondary cyclones. Another portion of the stripping steam and stripped hydrocarbons leaves the stripper through a conduit carrying spent catalyst to the regenerator. The bottom of the surge capacity means may be elevated, for example, by providing a serrated edge spacer in the wall of the conduit which supports the bottom of the surge capacity means in a spaced relationship with respect to the conduit and allows for the remaining portion of the stripping steam and stripped hydrocarbons to enter the enclosure.

The invention will now be described in connection with one specific embodiment thereof illustrated in Figures 1 and 2. This embodiment, however, is not to be construed as a limitation on the scope

of the invention. Referring to Figure 1, a reactor vessel 2 is provided with a catalyst stripping section 4 in a lower bottom portion of the vessel. The vessel 2 surrounds the terminal end of a riser conversion zone 6, to which are attached primary cyclone separating means 8 and 12, and secondary cyclones separating means 10 and 14, respectively. The primary cyclone separating means, or cyclones, 8 and 12 are attached by conduits 16 and 36, respectively, to the outlet of the riser conversion zone, or riser 6. The outlet of the primary cyclones 8 and 12 is attached to the secondary cyclones 10 and 14 by conduits 24 and 42, respectively, through a conventional expansion means, not shown in the drawings. It will be apparent to those skilled in the art that although only two pairs of the primary and secondary cyclones are shown in the embodiment of Figure 1, more than two pairs of the primary and secondary cyclones and/or more than two consecutive cyclone stages may be used in a commercial installation without impairing the operation of the apparatus and the process of the present invention. Cyclone separators 8 and 12 attached to the discharge end of riser 6 by conduit means 16 and 36 are provided with catalyst diplegs 18 and 40, provided with trickle valves 20 and 48 on the bottom discharge end thereof. Openings 22 and 38 are provided in conduits 16 and 36 to allow steam and/or hydrocarbon gases to enter conduits 16 and 36. Gasiform material separated in cyclones 8 and 12 passes through conduits 24 and 42 to secondary cyclones 10 and 14, wherein a further separation of catalyst fines from gaseous material is carried out. Separated catalyst is withdrawn by diplegs 26 and 44 from the secondary cyclones, and a gasiform material is passed from cyclones 10 and 14 by conduits 28 and 50 to a plenum chamber 30 for removal by conduit 32 and passage to a downstream fractionation equipment, not shown for clarity. The secondary cyclones 10 and 14 are provided with diplegs 26 and 44, which are provided with trickle valves 34 and 46 at the bottom end thereof.

The conduits 24 and 42 are provided with trickle valves 27 and 41, respectively, for accommodating sudden unexpected surges of increased pressure and of catalyst flow rate originating from operational or mechanical upsets. Alternatively, only conduits 16 and 36 may be provided with trickle valves 27A and 41A, respectively, to accommodate

the increased pressure and catalyst flow rate surges. In yet another embodiment, conduits 16, 24, 36 and 42 are provided with trickle valves 27A, 27, 41A and 41, respectively, as shown in Figure 1, to accommodate the increased pressure and catalyst flow rate surges. Figure 2 illustrates the detail of the valve 41, and it will be apparent to those skilled in the art that the valves 27, 27A and 41A are constructed and operated in the manner identical to that of valve 41. Referring to Figure 2, the gate 39 of the valve 41 is attached by a ring-hinge 43 to the conduit 42, thereby allowing the valve 41 to open in response to an increased pressure within the conduit 42. To open the valve 41, the pressure within the conduit 42 must exceed the pressure within the vessel 2 surrounding the conduit 42, and therefore the valve 41. Under normal operating conditions, the pressure within the conduit 42 does not exceed the pressure within vessel 2, and therefore the valve 41 remains closed. However, during sudden unexpected surges of flow of the catalyst and hydrocarbon suspension, or during unexpected pressure increases, as defined hereinbefore, pressure within the conduit 42 exceeds that in vessel 2 and forces valve 41 to open which allows the suddenly increased volume of the suspension to exit the conduit 42 through the opening and eliminate the excess material from the system. In the absence of the valve 41, an unexpected increased surge of the suspension flow may cause entrainment of a large proportion of catalyst within the cracked hydrocarbon stream, which, in turn, may cause excessive catalyst carryover to the FCC main fractionation column or damage to the internal apparatus of the fractionation column. The valve 41, or other surge capacity means, is sized to accommodate surges of up to 20 times of the steady state rate of catalyst flow. The bottom portion of valve plate 39 leans against the serrated edge 39A of the horizontal plate protruding from conduit 42. The serrated edge permits the stripping steam to enter conduit 42, thus preventing coke build-up on the edge of plate 39A which could partially or totally seal the valve 39.

The catalyst separated in diplegs 18, 26, 40 and 44 is discharged from the diplegs after a suitable pressure is generated within the diplegs by the buildup of the catalyst, and it falls into a bed of catalyst 52 therebelow. The bed 52 is contacted with a stream of gas,

such as steam, flowing countercurrently to the direction of flow of the catalyst. The gas is introduced into the lower bottom portion of the stripping section 4 by one or more conduits 54 and 56. Stripped catalyst is removed by a conduit 58 for passage to a catalyst regeneration zone or a second stage of hydrocarbon conversion zone, depending upon the activity and the amount of carbonaceous material, or coke, deposited on the catalyst particles.

The principal purpose of the enclosed conduits 36 and 42 is to provide a direct controlled passage of the cracked vapors from the riser reactor to the primary and secondary cyclones, and therefore to limit the time the cracked vapors are exposed to elevated cracking temperatures. Otherwise, the cracked vapors would pass randomly through the upper portion of vessel 4 to the cyclone separating means. This would provide additional opportunity for non-selective thermal cracking of the hydrocarbons, thereby lowering the product yield. By providing a direct enclosed path for the vapors to be transported out of the elevated temperature zone, there is provided an opportunity for the vapors to be quenched and fractionated in a controlled manner in the main fractionator of the processing unit, thereby limiting undesirable thermal overcracking.

Thus, in accordance with the present invention, the separation of catalyst from carbonaceous materials is achieved efficiently, while, at the same time, the length of time that the gaseous materials are subjected to high cracking reaction temperatures after separation from the catalysts is minimized. The direct connection between the primary and secondary cyclones provided by the enclosed conduits 16, 24, 36 and 42 is principally responsible for the reduction in thermal post-riser cracking. It will be apparent to those skilled in the art, that more than one surge capacity means, such as trickle valves 27, 27A, 41 and 41A, may be provided in the enclosed conduits 24, 16, 42 and 36, respectively.

In the method and apparatus of the present invention, a higher pressure is maintained outside of the primary cyclone than on the inside thereof. This causes a seal of catalyst to build up in the dipleg to a selected height depending on the pressure imposed on the system. The seal of catalyst in the dipleg substantially prevents the flow of

gasiform material into the dipleg. In contrast, in conventional prior art designs, the pressure inside the primary cyclone was maintained higher than the pressure outside of the cyclone. As a result, the gasiform hydrocarbon product had an opportunity to remain in contact with the catalyst for a longer time by being drawn down into the cyclone dipleg. In the process and apparatus of the present invention, the hydrocarbons exiting the primary cyclone enter the secondary cyclone directly through the conduits 24 and 42, respectively, and in the presence of a reduced amount of catalyst. In addition, the stripping steam and stripped hydrocarbons are generally at a lower temperature than the suspension of catalyst and cracked hydrocarbons passed to the primary cyclone, and the admixture of this lower temperature stripping steam and hydrocarbons in the primary and/or secondary cyclones considerably reduces overcracking and improves the separation of hydrocarbon vapors from catalyst particles in the suspension entering the cyclone.

In another embodiment of the invention, one or more of the primary cyclones, such as 8 and 12 as shown in Figure 1, may be modified to incorporate the stripping arrangement of the stripper cyclone of U.S. Patent 4,043,899. The employment of the stripper cyclone instead of the conventional primary cyclone shown in Figure 1 renders the operation even more effective for accomplishing the results desired insofar as hydrocarbon vapors flowing downwardly in the dipleg, in the interstitial volume between the catalyst particles, can be displaced by the stripping steam supplied to the stripper cyclone.

In one specific embodiment of the present invention, the process is conducted in such a manner that the pressure at the top of the riser reactor conduit is about 31.4 psig (318 kPa); the pressure within the reactor vessel 2 and outside of the riser is about 31.4 psig (318 kPa); the pressure within the first stage cyclone is about 30.5 psig (312 kPa); the pressure within the second stage cyclone is about 29.3 psig (303 kPa); and the pressure in the plenum chamber 30 is about 28.8 psig (300 kPa). Under these pressure operating conditions, it is estimated that the second stage cyclone dipleg will develop a catalyst seal in the dipleg of approximately 10 feet (3 meters) and a catalyst seal in the primary cyclone will be about 4.3 feet (1.3 meters).

It will be apparent to those skilled in the art that the specific embodiments discussed above can be successfully repeated with ingredients equivalent to those generically or specifically set forth above and under variable process conditions.

From the foregoing specification, one skilled in the art can readily ascertain the essential features of this invention and without departing from the spirit and scope thereof can adapt it to various diverse applications.

CLAIMS:

1. A process for the fluid catalytic cracking of a hydrocarbon feed, whereby the hydrocarbon feed is catalytically cracked, which process comprises:

- (a) passing a suspension of hydrocarbon feed and catalyst through riser cracking zone under cracking conditions,
- (b) separating the catalyst from the mixture of catalyst with the cracked hydrocarbons from the feed upon the discharge of such mixture as effluent from the riser cracking zone, said separating of the catalyst being accomplished by passing the effluent from the riser cracking zone through a first enclosed conduit means to a primary cyclone separation means and, subsequently, through a second enclosed conduit means to a secondary cyclone separation means, the second enclosed conduit means containing a surge capacity means to accommodate a sudden increased rate of flow of the effluent therethrough and sudden increase in pressure in the second enclosed conduit means;
- (c) substantially completely separating the catalyst from the cracked hydrocarbons in said primary and secondary cyclone separation means;
- (d) passing the thus-separated catalyst to a catalyst stripping zone wherein entrained hydrocarbons are removed from the catalyst with a stripping gas;
- (e) passing the cracked hydrocarbons to a downstream fractionation apparatus; and
- (f) passing the stripped catalyst to a catalyst regeneration vessel.

2. A process according to Claim 1 wherein the riser cracking zone, the primary and secondary cyclone separation means and conduit means thereto, and the catalyst stripping zone are housed within a single fluid catalytic cracking reactor vessel.
3. A process according to Claim 2 wherein the catalyst stripping zone is placed beneath said primary and secondary cyclone separation means.
4. A process according to any of Claims 1 to 3 wherein the first enclosed conduit means contains an opening which allows at least a portion of the stripping gas from the catalyst stripping zone to enter the first enclosed conduit means.
5. A process according to any of Claims 1 to 4 wherein the catalyst separated in said primary and said secondary cyclone separation means is conducted through a first and a second dipleg means, associated with the primary and secondary cyclone separation means, respectively, to the catalyst stripping zone.
6. A process according to any of Claims 1 to 5 wherein the sudden increased rate of flow of said effluent comprises a 2 to 20 times increase of the steady state rate of flow of said effluent.
7. A process according to any of Claims 1 to 6 wherein the first enclosed conduit means also contains a surge capacity means to accommodate a sudden increased rate of flow of the effluent therethrough and a sudden increase in pressure in the first enclosed conduit means.
8. A process according to any of Claims 1 to 7 wherein the means for accommodating surge capacity in the first and in the second enclosed conduits comprises an opening covered by a trickle valve means.

9. A process according to any of Claims 1 to 8 wherein the primary cyclone separation means is a stripper cyclone means and wherein the separation of the catalyst from the rising cracking zone effluent comprises
 - (a) passing the effluent from the riser cracking zone into a cyclonic separation zone wherein a first cyclonic separation is carried out between the fluid catalyst particles and cracked hydrocarbons from the feed;
 - (b) passing the catalyst particles thus separated substantially immediately into a lower separate portion of the stripper cyclone means through an opening into an annular zone wherein catalyst particles are contacted with a tangentially introduced stripping gas;
 - (c) passing the stripping gas and stripped products separated from the catalyst in the annular zone upwardly through an open end restricted passageway concentric with said annular zone and in open communication with an upper withdrawal passageway for removing cracked hydrocarbons from the feed from the upper portion of said stripper cyclone means into the second enclosed conduit means; and
 - (d) conducting the catalyst particles from the stripper cyclone means into the stripping zone.
10. Apparatus for the fluid catalytic cracking of a hydrocarbon feed, which apparatus comprises a reactor vessel which contains:
 - (a) a riser cracking zone comprising a vertically disposed elongated tubular conduit having an upstream end wherein a suspension of hydrocarbon feed and catalyst can be introduced and a downstream end from which an effluent comprising a mixture of catalyst and cracked hydrocarbons from the feed exits, said downstream end terminating within said reactor vessel;

- (b) a primary cyclone means connected to said downstream end of said riser cracking zone by a first enclosed conduit means, a secondary cyclone means connected to said primary cyclone means by a second enclosed conduit means, the second enclosed conduit means containing a surge capacity means to accommodate a sudden increased rate of flow of effluent therethrough, said primary and secondary cyclone means serving to separate catalyst material from said riser cracking zone effluent; and
 - (c) a catalyst stripping zone, wherein stripping gas is employed to remove entrained hydrocarbons from catalyst separated from said riser cracking zone effluent in said cyclone means.
- 11. Apparatus according to Claim 10 wherein said stripping zone is placed beneath said primary and secondary cyclone separation means.
 - 12. Apparatus according to Claim 10 or Claim 11 wherein said first enclosed conduit means contains an opening which allows at least a portion of the stripping gas from said catalyst stripping zone to enter said first enclosed conduit means.
 - 13. Apparatus according to any of Claims 10 to 12 wherein said primary and said secondary cyclone separation means separate said catalyst from said mixture and said separated catalyst is conducted through a first and a second dispieg means, associated with said primary and said secondary cyclone separation means, respectively, to said catalyst stripping zone.
 - 14. Apparatus according to any of Claims 10 to 13 wherein said first enclosed conduit means also contains a surge capacity means to accommodate a sudden increased rate of flow of effluent therethrough and a sudden increase in pressure in the first enclosed conduit means.

15. Apparatus according to Claim 14 wherein said means for accommodating surge capacity in said first and second enclosed conduit means comprises an opening covered by a trickle valve means.
16. Apparatus according to any of Claims 10 to 15 wherein said primary cyclone means is a stripper cyclone means and wherein said catalyst is separated from said riser cracking zone effluent by
 - (a) passing said effluent from said riser cracking zone into a cyclonic separation zone, wherein a first cyclonic separation is carried out between said catalyst and cracked hydrocarbons from the feed;
 - (b) passing the thus-separated catalyst substantially immediately into a lower separate portion of said stripper cyclone means through an opening into an annular zone wherein catalyst is contacted with a tangentially introduced stripping gas;
 - (c) passing said stripping gas and stripped products separated from said catalysts in said annular zone upwardly through an open end restricted passageway concentric with said annular zone and in open communication with an upper withdrawal passageway for removing cracked hydrocarbons from the feed from the upper portion of said stripper cyclone means into said second enclosed conduit means; and,
 - (d) conducting said catalyst from said stripper cyclone means into said stripping zone.

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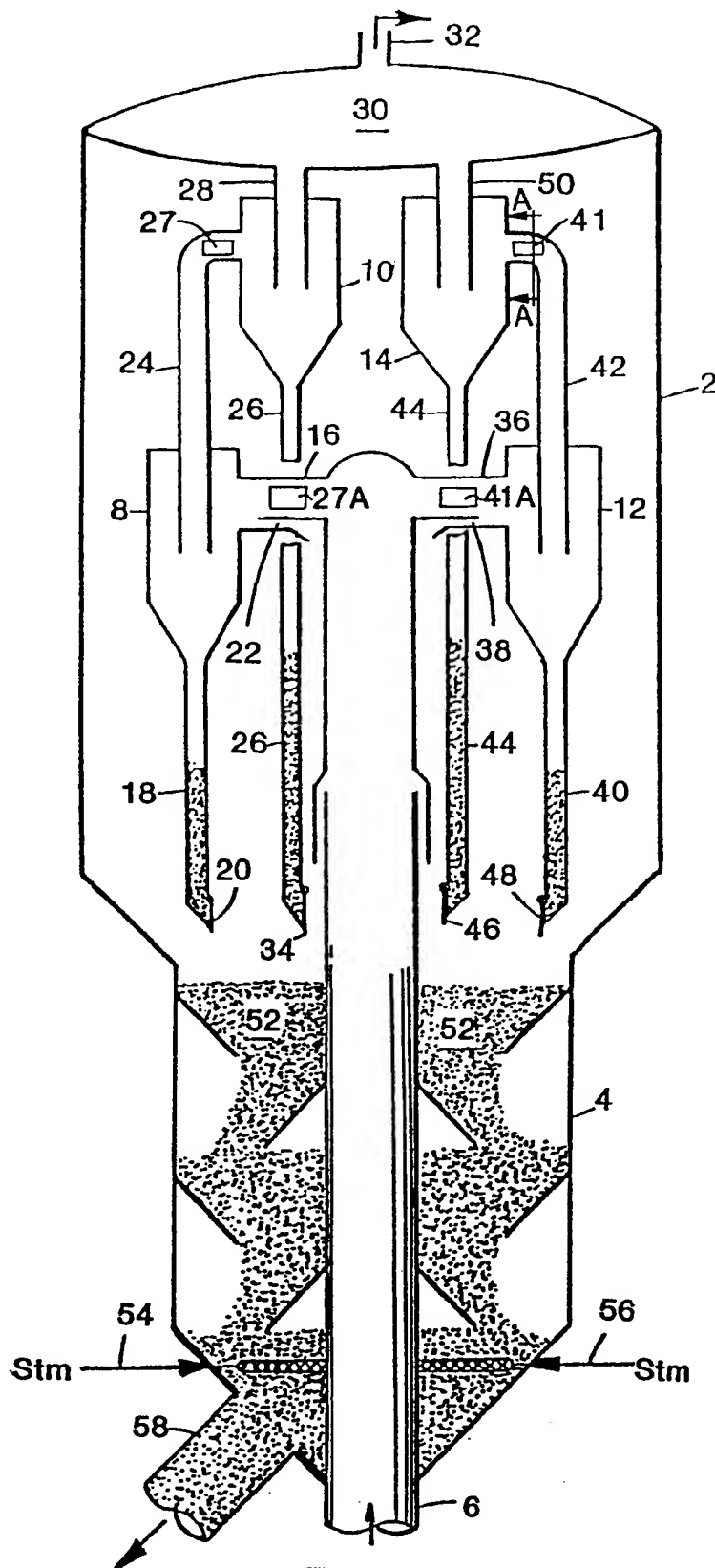


FIG. 1

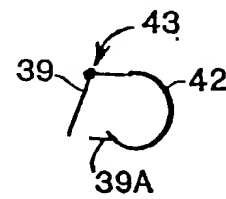


FIG. 2



European Patent
Office

EUROPEAN SEARCH REPORT

01 39392

Application number

DOCUMENTS CONSIDERED TO BE RELEVANT			EP 84305676.3
Category	Citation of document with indication, where appropriate, of relevant passages	Relevant to claim	CLASSIFICATION OF THE APPLICATION (Int. Cl. 4)
A	GB - A - 2 106 005 (STANDARD OIL COMPANY) * Claims; page 1, line 105 - page 2, line 34 * --	1,9,10	C 10 G 11/18
A	GB - A - 1 593 157 (MOBIL OIL CORPORATION) * Claims; page 2, lines 46-116 * --	1,9,10	
A	US - A - 4 385 985 (GROSS et al.) * Claims; column 3, lines 5-35 * --	1,9,10	
A	EP - A1 - 0 086 580 (MOBIL OIL CORPORATION) * Claims; pages 2-7 * ----	1,9,10	
The present search report has been drawn up for all claims			TECHNICAL FIELDS SEARCHED (Int. Cl. 4) C 10 G 11/00 B 04 C 5/00 B 01 D 45/00
Place of search VIENNA		Date of completion of the search 13-12-1984	Examiner STÖCKLMAYER
CATEGORY OF CITED DOCUMENTS X : particularly relevant if taken alone Y : particularly relevant if combined with another document of the same category A : technological background O : non-written disclosure P : intermediate document T : theory or principle underlying the invention E : earlier patent document, but published on, or after the filing date D : document cited in the application L : document cited for other reasons & : member of the same patent family, corresponding document			

(19)



Europäisches Patentamt

European Patent Office

Office européen des brevets

(11) Publication number:

0 139 392
B1

(12)

EUROPEAN PATENT SPECIFICATION

(45) Date of publication of patent specification: 07.01.88

(51) Int. Cl.⁴: **C 10 G 11/18**

(71) Application number: **84305676.3**

(22) Date of filing: **21.08.84**

(64) Closed reactor FCC system with provisions for surge capacity.

(30) Priority: **06.09.83 US 529824**

(43) Date of publication of application:
02.05.85 Bulletin 85/18

(5) Publication of the grant of the patent:
07.01.88 Bulletin 88/01

(64) Designated Contracting States:
BE DE FR GB IT NL

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GB-A-2 106 005
US-A-4 385 985

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EP 0 139 392 B1

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Courier Press, Leamington Spa, England.

Description

This invention relates to the separation of the catalyst phase from the gasiform phase in a fluidized catalytic cracking unit (FCC) reactor. More particularly, it relates to improvements in separating the catalyst phase from the gasiform phase, as the suspension comprising both phases is discharged from a riser conversion, i.e. riser cracking, zone outlet, to minimize or substantially eliminate post-riser conversion zone cracking.

The field of catalytic cracking, particularly fluid catalytic cracking, has undergone significant development improvements due primarily to advances in catalyst technology and product distribution obtained therefrom. With the advent of high activity catalysts and particularly crystalline zeolite cracking catalysts, new areas of operating technology have been encountered requiring even further refinements in processing techniques to take advantage of the high catalyst activity, selectivity and operating sensitivity.

Of particular concern in this field has been the development of methods and systems for separating gasiform products from fluidizable catalyst particles, particularly from a high activity crystalline zeolite cracking catalysts, under more efficient separating conditions so as to reduce the overcracking of conversion products and promote the recovery of desired products of a hydrocarbon conversion operation. However, present day cyclonic equipment often permits an undesired extended residence time of the product vapor within a large reactor vessel. This extended residence time causes a loss of the desired product yield of up to about 4 percent through non-selective thermal cracking. Recent developments in this art have been concerned with the rapid separation and recovery of entrained catalyst particles from gasiform products in a short contact time riser hydrocarbon conversion operation.

The hydrocarbon conversion catalyst usually employed in an FCC installation is preferably a high activity crystalline zeolite catalyst of a fluidizable particle size which is transferred in suspended or dispersed phase condition generally upwardly through one or more riser conversion zones providing a hydrocarbon residence time in each conversion zone in the range of 0.5 to about 10 seconds, and more usually less than about 8 seconds. High temperature riser hydrocarbon conversions of at least 1000°F (538°C) at 0.5 to 4 seconds hydrocarbon residence time in contact with the catalyst in the riser are desirable for some operations before initiating separation of vaporous hydrocarbon product materials from the catalyst. Rapid separation of catalyst from hydrocarbons discharged from a riser conversion zone is particularly desirable for restricting hydrocarbon conversion time. During the hydrocarbon conversion step, carbonaceous deposits accumulate on the catalyst particles and the particles entrain hydrocarbon vapors upon removal from the catalyst conversion step. The entrained hydrocarbons are subjected to further contact with the

catalyst until they are removed from the catalyst by mechanical means and/or stripping gas in a separate catalyst stripping zone. Hydrocarbon conversion products separated from the catalyst and stripped materials are combined and passed to a product fractionation step. Stripped catalyst containing deactivating amounts of carbonaceous material, hereinafter referred to as coke, is then passed to a catalyst regeneration operation.

Various processes and mechanical means have been employed heretofore to effect rapid separation of the catalyst phase from the hydrocarbon phase at the termination of the riser cracking zone, to minimize contact time of the catalyst with cracked hydrocarbons.

Cartmell, U.S.—A—3,661,799, discloses a process for catalytic conversion of petroleum feedstocks wherein the fluidized mixture of the cracking catalyst and cracked feedstock leaves a vertically-disposed reactor section and enters a cyclone separator, placed in a separate stripper vessel, through a conduit. The conduit contains an annulus which allows an inert stripping gas and associated stripped vapors to pass into the cyclone separator.

Anderson, et al., U.S.—A—4,043,899, disclose a method for rapid separation of a product suspension comprising fluidized catalyst particles and the vaporous hydrocarbon product phase by discharging the entire suspension directly from the riser conversion zone into a cyclonic separation zone which provides cyclonic stripping of the catalyst after it is separated from the hydrocarbon vapors. In the method of Anderson et al., the cyclone separator is modified to include an additional downwardly extending section comprising a lower cyclone stage. In this arrangement, catalyst separated from the gasiform material in the upper stage slides along a downwardly sloping baffle to the lower cyclone where stripping steam is introduced to further separate entrained hydrocarbon products from the catalyst recovered from the upper cyclone. The steam and the stripped hydrocarbons are passed from the lower cyclone through a concentric pipe where they are combined with the hydrocarbon vapors separated in the upper cyclone. The separated and stripped catalyst is collected and passes from the cyclone separator by conventional means through a dipleg. This process requires that the entire volume of catalyst, gasiform phase and stripping steam pass through the cyclone separator, which means that this equipment must be designed to efficiently handle not only a large vapor volume but also a large quantity of solid particles.

Myers et al., U.S.—A—4,070,159, provide a separation means whereby the bulk of the solids is discharged directly into the settling chamber without passing through a cyclone separator. In this apparatus, the discharge end of the riser conversion zone is in open communication with the disengaging chamber such that the catalyst discharges from the riser in a vertical direction into the disengaging chamber which is otherwise

essentially-closed to the flow of gases. The cyclone separation system is in open communication with the riser conversion zone by means of a port located upstream from but near the discharge end of the riser conversion zone. A deflector cone mounted directly above the terminus of the riser causes the catalyst to be directed in a downward path so as to prevent the catalyst from abrading the upper end of the disengaging vessel. The cyclone separator is of the usual configuration employed in a catalytic cracking unit to separate entrained catalyst particles from the cracked hydrocarbon products so that the catalyst passes through the dipleg of the cyclone to the body of the catalyst in the lower section of the disengaging vessel and the vaporous phase is directed from this vessel to a conventional fractionation unit. There is essentially no net flow of gases within the disengaging vessel beyond that resulting from a moderate amount of steam introduced to strip the catalyst residing in the bottom of the disengaging vessel.

Haddad et al., U.S.—A—4,219,407, the entire contents of which are incorporated herein by reference, disclose the separation of the catalyst from the gasiform cracked products in a fashion which permits effective steam stripping of the catalyst. The suspension of catalyst and gasiform material is discharged from the riser conversion zone outwardly through radially extending passageways, or arms, which terminate in a downward direction. Catalyst stripping zones, or strippers, are located beneath the terminus of each of the radially extending passageways. Each stripper consists of a vertical chamber open at the top and the bottom with downwardly sloping baffles located within the chamber so as to cause the catalyst to flow in a circuitous manner countercurrently to upwardly flowing stripping steam introduced at the lower end of the stripping chamber. The radially extending arms are each provided with a curved inner surface and confining sidewalls to impart a cyclonic concentration of catalyst particles promoting a forced separation thereof from the hydrocarbon vapors. The separation of the catalyst from the vapors is basically achieved through rapid changes in the direction of flow of the catalyst and the vapors. Thus the cyclonic collection and concentration of catalyst particles is used to reverse the flow of separated catalyst such that it is concentrated as a downwardly confined stream which discharges generally downwardly and into the open upper end of the catalyst stripping chamber. A vapor disengaging space is provided between the discharge end of the radially extending arms and the top of the catalyst strippers to promote the rapid removal of separated vapors from the catalyst. The separated vapors pass upwardly through the disengaging vessel to the open inlet of a cyclone separator which removes entrained catalyst from the gasiform material for return through a dipleg to the body of steam stripped catalyst while the separated vaporous material passes to a fractionation unit. The hydrocarbon product, as it

passes within the disengaging vessel from the discharge of the radially extending arms to the cyclone separator, travels in a random fashion and is exposed to catalytic reaction temperatures which may cause undesirable side reactions and thermal cracking before these vapors enter a quench zone in the main fractionator of the fluid cracking unit.

Haddad et al., U.S.—A—4,404,095, disclose an FCC reactor comprising a riser with radially extending sidearms as the first catalyst-hydrocarbon separation means. The sidearms force the suspension of the catalyst and the hydrocarbons to suddenly change the direction of flow from the vertical to the horizontal thereby forcing preliminary separation of the gaseous hydrocarbons from the solid catalyst particles. The catalyst particles fall in a downward direction, to a stripping means, while the hydrocarbons, with some entrained catalyst particles, proceed to a secondary separation means, such as a cyclone. The sidearms and the secondary separation means are enclosed by a vertical conduit to prevent random uncontrolled thermal cracking of the hydrocarbons. However, no means are provided in the apparatus and process of this patent for accommodating a sudden increase in pressure and the accompanying sudden increased rate of flow of the catalyst. Such unexpected increased pressure and the rate of flow of the cracking catalyst may be caused, for example, by mechanical malfunctions of equipment or by the vaporization of liquid water which may be introduced into the riser bottom with the hydrocarbon feed, or by unit pressure upsets.

It is a primary object of this invention to provide an improved process and apparatus for rapidly separating cracking catalyst from gasiform material and to provide an effective means of improving the ability of the FCC system to tolerate sudden system pressure increases and the accompanying surges in the catalyst rate of flow.

It is another object of this invention to provide an improved means for separating cracking catalyst from gasiform material in a fluid catalytic cracking (FCC) process.

It is a further object of this invention to provide a process and an apparatus for separating cracking catalyst from gasiform material whereby the length of time the gasiform material is subjected to high temperature after separation from the bulk of the catalyst is minimized so as to reduce non-selective thermal cracking of the vapor products.

These objectives can be realized in an improved FCC process and apparatus comprising a closed cyclone system for separating the catalyst from cracked hydrocarbon feed after the mixture of catalyst and feed exits the FCC cracking zone, e.g., the FCC riser. The system can be equipped with a means for providing a surge capacity to accommodate a sudden increased rate of flow of the catalyst stream. The closed cyclone system of the present invention comprises a primary cyclone means and a secondary cyclone means, or

primary and secondary cyclones. The primary cyclone is connected to the FCC cracking zone by an enclosed conduit. The secondary cyclone is placed in-series with the primary cyclone, and the outlet of the primary cyclone is also connected by an enclosed conduit with the inlet of the secondary cyclone. The enclosed conduits limit the exposure of the cracked hydrocarbons to the high temperatures of the FCC reactor, thereby expediting the transfer of cracked hydrocarbons to the secondary cyclone means and preventing undesirable post-riser thermal cracking of the hydrocarbons. The solid catalyst particles are separated as a catalyst stream from the hydrocarbon vapors in the two cyclone separation means. Most of the catalyst stream from the cyclones is then directed to a disengaging zone, e.g., a steam stripper, placed below the cyclones, and the hydrocarbon product is directed to a downstream fractionation means. In accordance with the present invention, surge capacity means is provided in the enclosed conduit connecting the riser with the primary cyclone, in the enclosed conduit connecting the primary with the secondary cyclone, or in both. These enclosed conduits connect the riser with the primary cyclone and the primary with the secondary cyclones.

The process and apparatus of this invention can be illustrated by the drawings which are described in greater detail hereinafter.

Figure 1 is a schematic representation of a side view of a fluid catalytic cracking (FCC) reactor of the present invention.

Figure 2 is the front view of the FCC reactor of the present invention, taken along the axis A—A of Figure 1.

The means for providing surge capacity to accommodate the sudden increased pressure and the sudden increased rate of flow of the catalyst stream can be, for example, a trickle valve which is positioned in one or both of the aforementioned enclosed conduits (e.g., see Figure 1). The trickle valve, or any other surge capacity means, is usually held closed by the higher pressure outside of the enclosed conduit than on the inside thereof. However, during the upset or surge conditions, the pressure inside the conduit exceeds that on the outside thereof forcing the surge capacity means to open and vent the excess material into the large reactor vessel surrounding the cyclones and the enclosed conduit. Therefore, in the event of a sudden unexpected surge of increased pressure and of the increased catalyst volume flow, the surge capacity means allows excess catalyst and hydrocarbon gases to exit the conduit, and the excess catalyst is deposited in the bottom of the reactor vessel. The provision of the surge capacity means prevents the primary and secondary cyclone dipleg flooding and large catalyst carryover from the FCC reactor to the main fractionation column, both of which might occur without the surge capacity means in the event of the surge conditions. In this connection, the term increased rate of catalyst flow, as used

herein and in the appended claims, designates a short term 2 to 20-fold increase of catalyst flow by volume per unit of time of the steady state rate of flow of the catalyst stream. Similarly, the term sudden increase in pressure designates the pressure increase inside the enclosed conduit of 2—10 psi (28—70 kPa), as compared to the steady state operating conditions. In a conduit connecting the riser of the FCC reactor and the primary cyclone, there is provided a means, e.g., a slotted opening, to provide an opportunity for the major portion of the stripping steam and stripped hydrocarbon mixtures to enter the inside of the conduit and therefore of the primary and secondary cyclones. Another portion of the stripping steam and stripped hydrocarbons leaves the stripper through a conduit carrying spent catalyst to the regenerator. The bottom of the surge capacity means may be elevated, for example, by providing a serrated edge spacer in the wall of the conduit which supports the bottom of the surge capacity means in a spaced relationship with respect to the conduit and allows for the remaining portion of the stripping steam and stripped hydrocarbons to enter the enclosure.

The invention will now be described in connection with one specific embodiment thereof illustrated in Figures 1 and 2. This embodiment, however, is not to be construed as a limitation on the scope of the invention. Referring to Figure 1, a reactor vessel 2 is provided with a catalyst stripping section 4 in a lower bottom portion of the vessel. The vessel 2 surrounds the terminal end of a riser conversion zone 6, to which are attached primary cyclone separating means 8 and 12, and secondary cyclones separating means 10 and 14, respectively. The primary cyclone separating means, or cyclones, 8 and 12 are attached by conduits 16 and 36, respectively, to the outlet of the riser conversion zone, or riser 6. The outlet of the primary cyclones 8 and 12 is attached to the secondary cyclones 10 and 14 by conduits 24 and 42, respectively, through a conventional expansion means, not shown in the drawings. It will be apparent to those skilled in the art that although only two pairs of the primary and secondary cyclones are shown in the embodiment of Figure 1, more than two pairs of the primary and secondary cyclones and/or more than two consecutive cyclone stages may be used in a commercial installation without impairing the operation of the apparatus and the process of the present invention. Cyclone separators 8 and 12 attached to the discharge end of riser 6 by conduit means 16 and 36 are provided with catalyst diplegs 18 and 40, provided with trickle valves 20 and 48 on the bottom discharge end thereof. Openings 22 and 38 are provided in conduits 16 and 36 to allow steam and/or hydrocarbon gases to enter conduits 16 and 36. Gasiform material separated in cyclones 8 and 12 passes through conduits 24 and 42 to secondary cyclones 10 and 14 wherein a further separation of catalyst fines from gaseous material is carried out. Separated catalyst is withdrawn by diplegs 26 and 44 from

the secondary cyclones, and a gasiform material is passed from cyclones 10 and 14 by conduits 28 and 50 to a plenum chamber 30 for removal by conduit 32 and passage to a downstream fractionation equipment, not shown for clarity. The secondary cyclones 10 and 14 are provided with diplegs 26 and 44, which are provided with trickle valves 34 and 46 at the bottom end thereof.

The conduits 24 and 42 are provided with trickle valves 27 and 41, respectively, for accommodating sudden unexpected surges of increased pressure and of catalyst flow rate originating from operational or mechanical upsets. Alternatively, only conduits 16 and 36 may be provided with trickle valves 27A and 41A, respectively, to accommodate the increased pressure and catalyst flow rate surges. In yet another embodiment, conduits 16, 24, 36 and 42 are provided with trickle valves 27A, 27, 41A and 41, respectively, as shown in Figure 1, to accommodate the increased pressure and catalyst flow rate surges. Figure 2 illustrates the detail of the valve 41, and it will be apparent to those skilled in the art that the valves 27, 27A and 41A are constructed and operated in the manner identical to that of valve 41. Referring to Figure 2, the gate 39 of the valve 41 is attached by a ring-hinge 43 to the conduit 42, thereby allowing the valve 41 to open in response to an increased pressure within the conduit 42. To open the valve 41, the pressure within the conduit 42 must exceed the pressure within the vessel 2 surrounding the conduit 42, and therefore the valve 41. Under normal operating conditions, the pressure within the conduit 42 does not exceed the pressure within vessel 2, and therefore the valve 41 remains closed. However, during sudden unexpected surges of flow of the catalyst and hydrocarbon suspension, or during unexpected pressure increases, as defined hereinbefore, pressure within the conduit 42 exceeds that in vessel 2 and forces valve 41 to open which allows the suddenly increased volume of the suspension to exit the conduit 42 through the opening and eliminate the excess material from the system. In the absence of the valve 41, an unexpected increased surge of the suspension flow may cause entrainment of a large proportion of catalyst within the cracked hydrocarbon stream, which, in turn, may cause excessive catalyst carryover to the FCC main fractionation column or damage to the internal apparatus of the fractionation column. The valve 41, or other surge capacity means, is sized to accommodate surges of up to 20 times of the steady state rate of catalyst flow. The bottom portion of valve plate 39 leans against the serrated edge 39A of the horizontal plate protruding from conduit 42. The serrated edge permits the stripping steam to enter conduit 42, thus preventing coke build-up on the edge of plate 39A which could partially or totally seal the valve 39.

The catalyst separated in diplegs 18, 26, 40 and 44 is discharged from the diplegs after a suitable pressure is generated within the diplegs by the buildup of the catalyst, and it falls into a bed of

catalyst 52 therebelow. The bed 52 is contacted with a stream of gas, such as steam, flowing countercurrently to the direction of flow of the catalyst. The gas is introduced into the lower bottom portion of the stripping section 4 by one or more conduits 54 and 56. Stripped catalyst is removed by a conduit 58 for passage to a catalyst regeneration zone or a second stage of hydrocarbon conversion zone, depending upon the activity and the amount of carbonaceous material, or coke, deposited on the catalyst particles.

The principal purpose of the enclosed conduits 36 and 42 is to provide a direct controlled passage of the cracked vapors from the riser reactor to the primary and secondary cyclones, and therefore to limit the time the cracked vapors are exposed to elevated cracking temperatures. Otherwise, the cracked vapors would pass randomly through the upper portion of vessel 4 to the cyclone separating means. This would provide additional opportunity for non-selective thermal cracking of the hydrocarbons, thereby lowering the product yield. By providing a direct enclosed path for the vapors to be transported out of the elevated temperature zone, there is provided an opportunity for the vapors to be quenched and fractionated in a controlled manner in the main fractionator of the processing unit, thereby limiting undesirable thermal overcracking.

Thus, in accordance with the present invention, the separation of catalyst from carbonaceous materials is achieved efficiently, while, at the same time, the length of time that the gaseous materials are subjected to high cracking reaction temperatures after separation from the catalysts is minimized. The direct connection between the primary and secondary cyclones provided by the enclosed conduits 16, 24, 36 and 42 is principally responsible for the reduction in thermal post-riser cracking. It will be apparent to those skilled in the art, that more than one surge capacity means, such as trickle valves 27, 27A, 41 and 41A, may be provided in the enclosed conduits 24, 16, 42 and 36, respectively.

In the method and apparatus of the present invention, a higher pressure is maintained outside of the primary cyclone than on the inside thereof. This causes a seal of catalyst to build up in the dipleg to a selected height depending on the pressure imposed on the system. The seal of catalyst in the dipleg substantially prevents the flow of gasiform material into the dipleg. In contrast, in conventional prior art designs, the pressure inside the primary cyclone was maintained higher than the pressure outside of the cyclone. As a result, the gasiform hydrocarbon product has an opportunity to remain in contact with the catalyst for a longer time by being drawn down into the cyclone dipleg. In the process and apparatus of the present invention, the hydrocarbons exiting the primary cyclone enter the secondary cyclone directly through the conduits 24 and 42, respectively, and in the presence of a reduced amount of a catalyst. In addition, the

stripping steam and stripped hydrocarbons are generally at a lower temperature than the suspension of catalyst and cracked hydrocarbons passed to the primary cyclone, and the admixture of this lower temperature stripping steam and hydrocarbons in the primary and/or secondary cyclones considerably reduces overcracking and improves the separation of hydrocarbon vapors from catalyst particles in the suspension entering the cyclone.

In another embodiment of the invention, one or more of the primary cyclones, such as 8 and 12 as shown in Figure 1, may be modified to incorporate the stripping arrangement of the stripper cyclone of U.S.—A—4,043,899. The employment of the stripper cyclone instead of the conventional primary cyclone shown in Figure 1 renders the operation even more effective for accomplishing the results desired insofar as hydrocarbon vapors flowing downwardly in the dipleg, in the interstitial volume between the catalyst particles, can be displaced by the stripping steam supplied to the stripper cyclone.

In one specific embodiment of the present invention, the process is conducted in such a manner that the pressure at the top of the riser reactor conduit is about 31.4 psig (318 kPa); the pressure within the reactor vessel 2 and outside of the riser is about 31.4 psig (318 kPa); the pressure within the first stage cyclone is about 30.5 psig (312 kPa); the pressure within the second stage cyclone is about 29.3 psig (303 kPa); and the pressure in the plenum chamber 30 is about 28.8 psig (300 kPa). Under these pressure operating conditions, it is estimated that the second stage cyclone dipleg will develop a catalyst seal in the dipleg of approximately 10 feet (3 meters) and a catalyst seal in the primary cyclone will be about 4.3 feet (1.3 meters).

It will be apparent to those skilled in the art that the specific embodiments discussed above can be successfully repeated with ingredients equivalent to those generically or specifically set forth above and under variable process conditions.

Our EP 84305675 (published EP—A—139,391) discloses an FCC riser reactor equipped with an opening which allows stripping gases from a catalyst stripping zone to enter the riser. The pressure in a reactor vessel containing the riser reactor is higher than the pressure inside the FCC riser reactor, and downstream cyclones associated with the riser reactor. This changed pressure relationship decreases the amount of uncontrolled post-riser cracking within the reactor vessel.

Claims

1. A process for the fluid catalytic cracking of a hydrocarbon feed, whereby the hydrocarbon feed is catalytically cracked, which process comprises:

(a) passing a suspension of hydrocarbon feed and catalyst through riser cracking zone (6) under cracking conditions,

(b) separating the catalyst from the mixture of

catalyst with the cracked hydrocarbons from the feed upon the discharge of such mixture as effluent from the riser cracking zone (6), said separating of the catalyst being accomplished by passing the effluent from the riser cracking zone (6) through a first enclosed conduit means (16, 36) to a primary cyclone separation means (8, 12) and, subsequently, through a second enclosed conduit means (24, 42) to a secondary cyclone separation means (10, 14), at least one of the enclosed conduit means (16, 36, 24, 42) containing a surge capacity means (27A, 41A, 27, 41) to accommodate a sudden increased rate of flow of the effluent therethrough and sudden increase in pressure;

(c) substantially completely separating the catalyst from the cracked hydrocarbons in said primary (8, 12) and secondary (10, 14) cyclone separation means;

(d) passing the thus-separated catalyst to a catalyst stripping zone (4) wherein entrained hydrocarbons are removed from the catalyst with a stripping gas;

(e) passing the cracked hydrocarbons to a downstream fractionation apparatus; and

(f) passing the stripped catalyst to a catalyst regeneration vessel.

2. A process according to Claim 1 wherein the riser cracking zone (6), the primary (8, 12) and secondary (10, 14) cyclone separation means and conduit means thereto (16, 36, 24, 42), and the catalyst stripping zone (4) are housed within a single fluid catalytic cracking reactor vessel.

3. A process according to Claim 2 wherein the catalyst stripping zone (4) is placed beneath said primary (8, 12) and secondary (10, 14) cyclone separation means.

4. A process according to any of Claims 1 to 3 wherein the first enclosed conduit means (16, 36) contains an opening (22, 38) which allows at least a portion of the stripping gas from the catalyst stripping zone to enter the first enclosed conduit means.

5. A process according to any of Claims 1 to 4 wherein the catalyst separated in said primary (8, 12) and said secondary (10, 14) cyclone separation means is conducted through a first (18, 40) and a second (26, 44) dipleg means, associated with the primary and secondary cyclone separation means, respectively, to the catalyst stripping zone.

6. A process according to any of Claims 1 to 5 wherein the sudden increased rate of flow of said effluent comprises a 2 to 20 times increase of the steady state rate of flow of said effluent.

7. A process according to any of Claims 1 to 6 wherein both the first (16, 36) and the second (24, 42) enclosed conduit means contain a surge capacity means (27A, 41A, 27, 41).

8. A process according to any of Claims 1 to 7 wherein the means for accommodating surge capacity in the first (16, 36) and in the second (24, 42) enclosed conduits comprises an opening covered by a trickle valve means.

9. A process according to any of Claims 1 to 8

wherein the primary cyclone separation means (8, 12) is a stripper cyclone means and wherein the separation of the catalyst from the rising cracking zone effluent comprises

(a) passing the effluent from the riser cracking zone (6) into a cyclonic separation zone (8, 12) wherein a first cyclonic separation is carried out between the fluid catalyst particles and cracked hydrocarbons from the feed;

(b) passing the catalyst particles thus separated substantially immediately into a lower separate portion of the stripper cyclone means through an opening into an annular zone wherein catalyst particles are contacted with a tangentially introduced stripping gas;

(c) passing the stripping gas and stripped products separated from the catalyst in the annular zone upwardly through an open end restricted passageway concentric with said annular zone and in open communication with an upper withdrawal passageway for removing cracked hydrocarbons from the feed from the upper portion of said stripper cyclone means into the second enclosed conduit means; and

(d) conducting the catalyst particles from the stripper cyclone means into the stripping zone.

10. Apparatus for the fluid catalytic cracking of a hydrocarbon feed, which apparatus comprises a reactor vessel (2) which contains:

(a) a riser cracking zone (6) comprising a vertically disposed elongated tubular conduit having an upstream end wherein a suspension of hydrocarbon feed and catalyst can be introduced and a downstream end from which an effluent comprising a mixture of catalyst and cracked hydrocarbons from the feed exits, said downstream end terminating within said reactor vessel;

(b) a primary cyclone means (8, 12) connected to said downstream end of said riser cracking zone by a first enclosed conduit means (16, 36), a secondary cyclone means (10, 14) connected to said primary cyclone means by a second enclosed conduit means (24, 42) and at least one of the enclosed conduit means containing a surge capacity means (27A, 41A, 27, 41) to accommodate a sudden increased rate of flow of effluent therethrough, said primary (8, 12) and secondary (10, 14) cyclone means serving to separate catalyst material from said riser cracking zone effluent; and

(c) a catalyst stripping zone (4), wherein stripping gas is employed to remove entrained hydrocarbons from catalyst separated from said riser cracking zone effluent in said cyclone means.

11. Apparatus according to Claim 10 wherein said stripping zone (4) is placed beneath said primary (8, 12) and secondary (10, 14) cyclone separation means.

12. Apparatus according to Claim 10 or Claim 11 wherein said first enclosed conduit means (16, 36) contains an opening (22, 38) which allows at least a portion of the stripping gas from said catalyst stripping zone (4) to enter said first enclosed conduit means.

13. Apparatus according to any of Claims 10 to

12 wherein said primary (8, 12) and said secondary (10, 14) cyclone separation means separate said catalyst from said mixture and said separated catalyst is conducted through a first (18, 40) and a second (26, 44) dipleg means, associated with said primary and said secondary cyclone separation means, respectively, to said catalyst stripping zone (4).

14. Apparatus according to any of Claims 10 to 13 wherein both said first (16, 36) and said second (24, 42) enclosed conduit means contain a surge capacity means (27A, 41A, 27, 41).

15. Apparatus according to Claim 14 wherein said means for accommodating surge capacity in said first (16, 36) and second (24, 42) enclosed conduit means comprises an opening covered by a trickle valve means.

16. Apparatus according to any of Claims 10 to 15 wherein said primary cyclone means (8, 12) is a stripper cyclone means and wherein said catalyst is separated from said riser cracking zone effluent by

(a) passing said effluent from said riser cracking zone into a cyclonic separation zone, wherein a first cyclonic separation is carried out between said catalyst and cracked hydrocarbons from the feed;

(b) passing the thus-separated catalyst substantially immediately into a lower separate portion of said stripper cyclone means through an opening into an annular zone wherein catalyst is contacted with a tangentially introduced stripping gas;

(c) passing said stripping gas and stripped products separated from said catalysts in said annular zone upwardly through an open end restricted passageway concentric with said annular zone and in open communication with an upper withdrawal passageway for removing cracked hydrocarbons from the feed from the upper portion of said stripper cyclone means into said second enclosed conduit means; and

(d) conducting said catalyst from said stripper cyclone means into said stripping zone.

Patentansprüche

1. Verfahren zum katalytischen Wirbelschichtcracken einer Kohlenwasserstoffzufuhr, wodurch die Kohlenwasserstoffzufuhr katalytisch ge crackt wird, wobei das Verfahren umfaßt:

a) Leiten einer Suspension der Kohlenwasserstoffzufuhr und des Katalysators durch eine Riser crackzone (6) unter Crackbedingungen,

b) Abtrennen des Katalysators aus der Mischung des Katalysators mit den ge crackten Kohlenwasserstoffen aus der Zufuhr während des Ablassens dieser Mischung als Abfluß aus der Riser crackzone (6), wobei das Abtrennen des Katalysators durch Leiten dieses Abflusses aus der Riser crackzone (6) durch eine erste eingeschlossene Leitungseinrichtung (16, 36) zu einer primären Zyklonabtrenneinrichtung (8, 12) und nachfolgend durch eine zweite eingeschlossene Leitungseinrichtung (24, 42) zu

einer sekundären Zyklonabtrenneinrichtung (10, 14) durchgeführt wird, wobei zumindest eine der eingeschlossenen Leitungseinrichtungen (16, 36, 24, 42) eine Überschußkapazitätseinrichtung (27A, 41A, 27, 41) enthält, um eine plötzlich erhöhte Strömungsgeschwindigkeit des Abflusses durch diese hindurch und eine plötzliche Druckerhöhung anzupassen,

c) im wesentlichen vollständige Abtrennung des Katalysators von den gecrackten Kohlenwasserstoffen in der ersten (8, 12) und zweiten (10, 14) Zyklonabtrenneinrichtung,

d) Leiten des so abgetrennten Katalysators zur Katalysatorabstreifzone (4), worin eingetretene Kohlenwasserstoffe mit Abstreifgas vom Katalysator entfernt werden,

e) Leiten der gecrackten Kohlenwasserstoffe zu einer stromabwärtigen Fraktionier Vorrichtung und

f) Leiten des abgestreiften Katalysators zu einem Katalysatorregeneriergefäß.

2. Verfahren nach Anspruch 1, worin die Riser-crackzone (6) die primäre (8, 12) und sekundäre (10, 14) Zyklonabtrenneinrichtung und Leitungseinrichtung dahin (16, 36, 24, 42) und die Katalysatorabstreifzone (4) innerhalb eines einzelnen katalytischen Wirbelschichtcrack-Reaktor-gefaßes enthalten sind.

3. Verfahren nach Anspruch 2, worin die Katalysatorabstreifzone (4) unter der primären (8, 12) und sekundären (10, 14) Zyklonabtrenneinrichtung angeordnet ist.

4. Verfahren nach einem der Ansprüche 1 bis 3, worin die erste eingeschlossene Leitungseinrichtung (16, 36) eine Öffnung (22, 38) enthält, die gestattet, daß zumindest ein Teil des Abstreifgases von der Katalysatorabstreifzone in die erste eingeschlossene Leitungseinrichtung eintritt.

5. Verfahren nach einem der Ansprüche 1 bis 4, worin der Katalysator, der in der ersten (8, 12) und zweiten (10, 14) Zyklonabtrenneinrichtung abgetrennt wurde, durch eine erste (18, 40) und zweite (26, 44) Tauchleitungseinrichtung, die mit der primären bzw. sekundären Zyklonabtrenneinrichtung verbunden ist, zur Katalysatorabstreifzone geführt wird.

6. Verfahren nach einem der Ansprüche 1 bis 5, worin die plötzlich erhöhte Strömungsgeschwindigkeit des Abflusses eine zwei bis zwanzigfache Erhöhung der Strömungsgeschwindigkeit des Abflusses im Dauerzustand umfaßt.

7. Verfahren nach einem der Ansprüche 1 bis 6, worin sowohl die erste (16, 36) als auch zweite (24, 42) eingeschlossene Leitungseinrichtung eine Überschußkapazitätseinrichtung (27A, 41A, 27, 41) umfaßt.

8. Verfahren nach einem der Ansprüche 1 bis 7, worin die Einrichtung zum Anpassen der Überschußkapazität in der ersten (16, 36) und in der zweiten (24, 42) eingeschlossenen Leitung eine Öffnung umfaßt, die mit einer Rieselventileinrichtung abgedeckt ist.

9. Verfahren nach einem der Ansprüche 1 bis 8, worin die erste Zyklonabtrenneinrichtung (8, 12)

eine Zyklonabstreifeinrichtung ist und worin die Abtrennung des Katalysators von dem Abfluß der Riser-crackzone umfaßt;

a) Leiten des Abflusses von der Riser-crackzone (6) in eine Zyklonabtrennzone (8, 12), worin eine erste Zyklonabscheidung zwischen den Katalysatorfluidpartikeln und den gecrackten Kohlenwasserstoffen aus der Zufuhr durchgeführt wird,

b) Leiten der so abgetrennten Katalysatorpartikel im wesentlichen unmittelbar in einen unteren getrennten Abschnitt der Zyklonabstreifeinrichtung durch eine Öffnung in eine ringförmige Zone, worin die Katalysatorpartikel mit dem tangential eingeführten Abstreifgas in Kontakt gebracht werden,

c) Leiten des Abstreifgases und der abgestreiften Produkte, die vom Katalysator in der ringförmigen Zone abgetrennt wurden, nach oben durch ein offenes Ende des begrenzten Durchganges, der mit der ringförmigen Zone konzentrisch ist und in offener Verbindung mit einem oberen Abzugsdurchgang steht, um die gecrackten Kohlenwasserstoffe von der Zufuhr aus dem oberen Abschnitt der Zyklonabstreifeinrichtung in die zweite eingeschlossene Leitungseinrichtung zu entfernen und

d) Leiten der Katalysatorpartikel aus der Zyklonabstreifeinrichtung in die Abstreifzone.

10. Vorrichtung zum katalytischen Wirbelschichtcracken einer Kohlenwasserstoffzufuhr, wobei die Vorrichtung ein Reaktor-gefäß (2) umfaßt, welches enthält:

a) eine Riser-crackzone (6), die eine vertikal angeordnete, verlängerte röhrenförmige Leitung mit einem stromabwärtigen Ende, worin eine Suspension der Kohlenwasserstoffzufuhr und des Katalysators eingegeben werden kann und einem stromabwärtigen Ende umfaßt, aus dem der Abfluß, der eine Mischung des Katalysators und der gecrackten Kohlenwasserstoffe aus der Zufuhr umfaßt, austritt, wobei das stromabwärtige Ende innerhalb des Reaktor-gefäßes abschließt,

b) eine primäre Zykloneinrichtung (8, 12), die durch eine erste eingeschlossene Leitungseinrichtung (16, 36) an das stromabwärtige Ende der Riser-crackzone verbunden ist, eine sekundäre Zykloneinrichtung (10, 14), die durch eine zweite eingeschlossene Leitungseinrichtung (24, 42) an die primäre Zykloneinrichtung verbunden ist und zumindest eine der eingeschlossenen Leitungseinrichtungen eine Überschußkapazitätseinrichtung (27A, 41A, 27, 41) enthält, um eine plötzlich erhöhte Strömungsgeschwindigkeit des Abflusses durch diese hindurch anzupassen, wobei die primäre (8, 12) und sekundäre (10, 14) Zykloneinrichtung dazu dient, das Katalysatormaterial vom Abfluß der Riser-crackzone abzutrennen und

c) eine Katalysatorabstreifzone (4), worin Abstreifgas verwendet wird, um eingetretene Kohlenwasserstoffe vom Katalysator zu entfernen, der in der Zykloneinrichtung vom Abfluß der Riser-crackzone abgetrennt wurde.

11. Vorrichtung nach Anspruch 10, worin die Abstreifzone (4) unter der primären (8, 12) und sekundären (10, 14) Zyklonabtrenneinrichtung angeordnet ist.

12. Vorrichtung nach Anspruch 10 oder 11, worin die erste eingeschlossene Leitungseinrichtung (16, 36) eine Öffnung (22, 38) enthält, die gestattet, daß zumindest ein Teil des Abstreifgases aus der Katalysatorabstreifzone (4) in die erste eingeschlossene Leitungseinrichtung eintritt.

13. Vorrichtung nach einem der Ansprüche 10 bis 12, worin die primäre (8, 12) und sekundäre (10, 14) Zyklonabtrenneinrichtung den Katalysator von dieser Mischung abtrennt und der abgetrennte Katalysator durch eine erste (18, 40) und zweite (26, 44) Tauchleitungseinrichtung, die mit der primären bzw. sekundären Zyklonabtrenneinrichtung verbunden ist, zur Katalysatorabstreifzone (4) geleitet wird.

14. Vorrichtung nach einem der Ansprüche 10 bis 13, worin sowohl die erste (16, 36) als auch die zweite (24, 42) eingeschlossene Leitungseinrichtung eine Überschußkapazitätseinrichtung (27A, 41A, 27, 41) enthält.

15. Vorrichtung nach Anspruch 14, worin die Einrichtung zur Ausgleichung der Überschußkapazität in der ersten (16, 36) und zweiten (24, 42) eingeschlossenen Leitungseinrichtung eine Öffnung umfaßt, die durch eine Rieselsventileinrichtung abgedeckt ist.

16. Vorrichtung nach einem der Ansprüche 10 bis 15, worin die primäre Zykloleinrichtung (8, 12) eine Zyklonabstreifeinrichtung ist und worin der Katalysator vom Abfluß der Riser-crackzone durch,

a) Leiten des Abflusses aus der Riser-crackzone in eine Zyklonabtrennzone, worin eine erste Zyklonabtrennung zwischen dem Katalysator und den gecrackten Kohlenwasserstoffen aus der Zufuhr durchgeführt wird,

b) Leiten des so abgetrennten Katalysators im wesentlichen unmittelbar in einen unteren abgetrennten Abschnitt der Zyklonabstreifeinrichtung durch eine Öffnung in eine ringförmige Zone, worin der Katalysator mit einem tangential eingeführten Abstreifgas in Kontakt gebracht wird,

c) Leiten des Abstreifgases und der abgestreiften Produkte, die in der ringförmigen Zone vom Katalysator abgetrennt wurden, nach oben durch ein offenes Ende des begrenzten Durchganges, der mit der ringförmigen Zone konzentrisch ist und in offener Verbindung mit einem oberen Abzugsdurchgang steht, um die gecrackten Kohlenwasserstoffe von der Zufuhr vom oberen Abschnitt der Zyklonabstreifeinrichtung in die untere eingeschlossene Leitungseinrichtung zu entfernen und

d) Leiten des Katalysators aus der Zyklonabstreifeinrichtung in die Abstreifzone abgetrennt wird.

Revendications

1. Procédé de craquage catalytique en lit fluid-

disé d'une charge hydrocarbonée, dans lequel on craque la charge hydrocarbonée par voie catalytique, ce procédé comprenant les étapes consistant à:

(a) faire passer une charge de la suspension formée de la charge hydrocarbonée et du catalyseur au travers d'une zone de craquage ascendante (6) dans des conditions de craquage;

(b) séparer le catalyseur du mélange de catalyseur et des hydrocarbures craqués produits par la charge après que ce mélange quitte en tant qu'effluent la zone de craquage ascendante (6), cette séparation étant réalisée par passage de l'effluent de la zone de craquage ascendante (6) par des premiers conduits protégés (16, 36) et des moyens primaires de séparation cycloniques (8, 12) et ensuite par des seconds conduits protégés (24, 42) puis des moyens secondaires de séparation cycloniques (10, 14), au moins l'un des conduits protégés (16, 36, 24, 42) contenant des moyens antisurcharge (27A, 41A, 27, 41) pour faire face à un accroissement soudain du débit de l'effluent et à un soudain accroissement de pression;

(c) séparer de façon sensiblement complète le catalyseur des hydrocarbures craqués dans lesdits moyens de séparation cycloniques primaires (8, 12) et secondaires (10, 14);

(d) transférer le catalyseur ainsi séparé vers une zone d'extraction de catalyseur (4) dans laquelle les hydrocarbures entraînés sont retirés du catalyseur à l'aide d'un gaz d'extraction;

(e) amener les hydrocarbures craqués à un dispositif de fractionnement en aval; et

(f) faire passer le catalyseur recueilli par extraction à une cuve de régénération de catalyseur.

2. Procédé selon la revendication 1, dans lequel la zone de craquage ascendante (6), les moyens de séparation cycloniques primaires (8, 12) et secondaires (10, 14), les conduits (16, 36, 24, 42) et la zone d'extraction du catalyseur (4) sont longés dans une cuve unique formant le réacteur de craquage catalytique à lit fluidisé.

3. Procédé selon la revendication 2, dans lequel la zone (4) d'extraction de catalyseur est située en dessous desdits moyens de séparation cycloniques primaires (8, 12) et secondaires (10, 14).

4. Procédé selon l'une quelconque des revendications 1 à 3, dans lequel les premiers conduits protégés (16, 36) présentent une ouverture (22, 38) permettant au moins à une partie du gaz d'extraction provenant de la zone d'extraction de catalyseur d'entrer dans les premiers conduits protégés.

5. Procédé selon l'une quelconque des revendications 1 à 4, dans lequel le catalyseur séparé dans lesdits moyens de séparation cycloniques primaires (8, 12) et secondaires (10, 14) est amené par des premiers (18, 40) et second (26, 44) tubes plongeurs, associés à des moyens de séparation cycloniques primaires et secondaires respectivement, à une zone d'extraction de catalyseur.

6. Procédé selon l'une quelconque des revendications 1 à 5, dans lequel l'accroissement sou-

dain de débit dudit effluent représente de 2 à 20 fois le débit normal de cet effluent.

7. Procédé selon l'une quelconques des revendications 1 à 6, dans lequel les premiers (16, 36) et les seconds (24, 42) conduits protégés comportent tous deux des moyens antisurcharge (27A, 41A, 27, 41).

8. Procédé selon l'une quelconques des revendications 1 à 7, dans lequel les moyens permettant de faire face à une surcharge dans les premiers (16, 36) et dans les seconds (24, 42) conduits protégés comprennent une ouverture clôturée par une vanne goutte à goutte.

9. Procédé selon l'une quelconques des revendications 1 à 8, dans lequel les premiers moyens de séparation cycloniques (8, 12) sont formés de cyclones d'extraction et dans lequel la séparation du catalyseur de l'effluent dans la zone de craquage ascendante comprend les étapes consistant à:

(a) faire passer l'effluent de la zone de craquage ascendante (6) à une zone de séparation cyclonique (8, 12) dans laquelle une première séparation cyclonique est effectuée entre les particules de catalyseur fluidisées et les hydrocarbures craqués produits par la charge;

(b) faire passer les particules de catalyseur ainsi séparées presque immédiatement dans une partie inférieure distincte des cyclones d'extraction par une ouverture dans une zone annulaire où les particules de catalyseur entrent en contact avec un gaz d'extraction introduit tangentiellement;

(c) faire passer le gaz d'extraction et les produits extraits séparés du catalyseur dans la zone annulaire vers le haut par un passage libre à extrémité rétrécie qui est concentrique à ladite zone annulaire et en libre communication avec un passage supérieur de décharge pour retirer les hydrocarbures craqués de la charge dans la partie supérieure desdits moyens cycloniques d'extraction et les amener dans les seconds moyens de conduit protégés; et

(d) faire passer les particules de catalyseur des moyens cycloniques d'extraction dans la zone d'extraction.

10. Dispositif pour le craquage catalytique à lit fluidisé d'une charge d'hydrocarbures, comprenant une cuve de réaction ou réacteur (2) qui contient:

(a) une zone de craquage ascendante (6) comprenant un conduit tubulaire allongé vertical ayant une extrémité amont dans laquelle peut être introduite une suspension de charge hydrocarbonée et de catalyseur et une extrémité aval de laquelle sort un effluent comprenant un mélange de catalyseur et d'hydrocarbures craqués produits à partir de la charge, cette extrémité aval se terminant dans ladite cuve de réacteur;

(b) des moyens de cyclone primaires (8, 12) reliés à l'extrémité aval de ladite zone de craquage ascendante par des premiers conduits protégés (16, 36), reliés à des moyens cycloniques secondaires (10, 14) reliés auxdits moyens cycloniques primaires par des seconds conduits protégés (24, 42) et au moins un des conduits

protégés contenant des moyens antisurcharge (27A, 41A, 27, 41) pour faire face à un accroissement subit du débit de l'effluent qui les traversent, lesdits moyens cycloniques primaires (8, 12) et secondaires (10, 14) servant à séparer le catalyseur de l'effluent de la zone de craquage ascendante; et

(c) une zone d'extraction de catalyseur (4) dans laquelle un gaz d'extraction retire les hydrocarbures entraînés du catalyseur séparé de l'effluent de la zone de craquage ascendante dans lesdits moyens cycloniques.

11. Dispositif selon la revendication 10, dans lequel ladite zone d'extraction (4) est placée en dessous desdits moyens de séparation cycloniques primaires (8, 12) et secondaires (10, 14).

12. Dispositif selon la revendication 10 ou 11, dans lequel les premiers conduits protégés (16, 36) présentent une ouverture (22, 38) permettant au moins à une partie du gaz d'extraction provenant de la zone d'extraction du catalyseur d'entrer dans les premiers conduits protégés.

13. Dispositif selon l'une quelconque des revendications 10 à 12, dans lequel lesdits moyens de séparation cycloniques primaires (8, 12) et secondaires (10, 14) séparent ledit catalyseur dudit mélange et ledit catalyseur séparé est amené par des premiers (18, 40) et seconds (26, 44) tubes plongeurs, associés à des moyens de séparation cycloniques primaires et secondaires respectivement, à ladite zone d'extraction de catalyseur (4).

14. Dispositif selon l'une quelconque des revendications 10 à 13, dans lequel les premiers (16, 36) et les seconds (24, 42) conduits protégés comportent tous deux des moyens antisurcharge (27A, 41A, 27, 41).

15. Dispositif selon la revendication 14, dans lequel les moyens permettant de faire face à une surcharge dans les premiers (16, 36) et dans les seconds (24, 42) conduits protégés comprennent une ouverture clôturée par une vanne goutte à goutte.

16. Dispositif selon l'une quelconque des revendications 10 à 15, dans lequel les moyens cycloniques primaires (8, 12) sont des cyclones d'extraction et dans lequel ledit catalyseur est séparé de l'effluent dans la zone de craquage ascendante par les étapes consistant à:

(a) faire passer ledit effluent de la zone de craquage ascendante dans une zone de séparation cyclonique dans laquelle une première séparation cyclonique est effectuée entre le catalyseur et les hydrocarbures craqués produits à partir de la charge;

(b) faire passer le catalyseur ainsi séparé presque immédiatement dans une partie inférieure distincte des moyens cycloniques d'extraction par une ouverture dans une zone annulaire et où le catalyseur est mis au contact d'un gaz d'extraction introduit tangentiellement;

(c) faire passer ledit gaz d'extraction et lesdits produits extraits séparés du catalyseur dans une zone annulaire vers le haut à travers un passage libre à extrémité rétrécie qui est concentrique

avec ladite zone annulaire et en communication libre avec un passage supérieur de décharge pour retirer les hydrocarbures craqués produits par la charge par la partie supérieure desdits moyens de

cycloniques d'extraction et les amener dans lesdits conduits protégés; et

(d) faire passer ledit catalyseur des moyens cycloniques d'extraction à la zone d'extraction.

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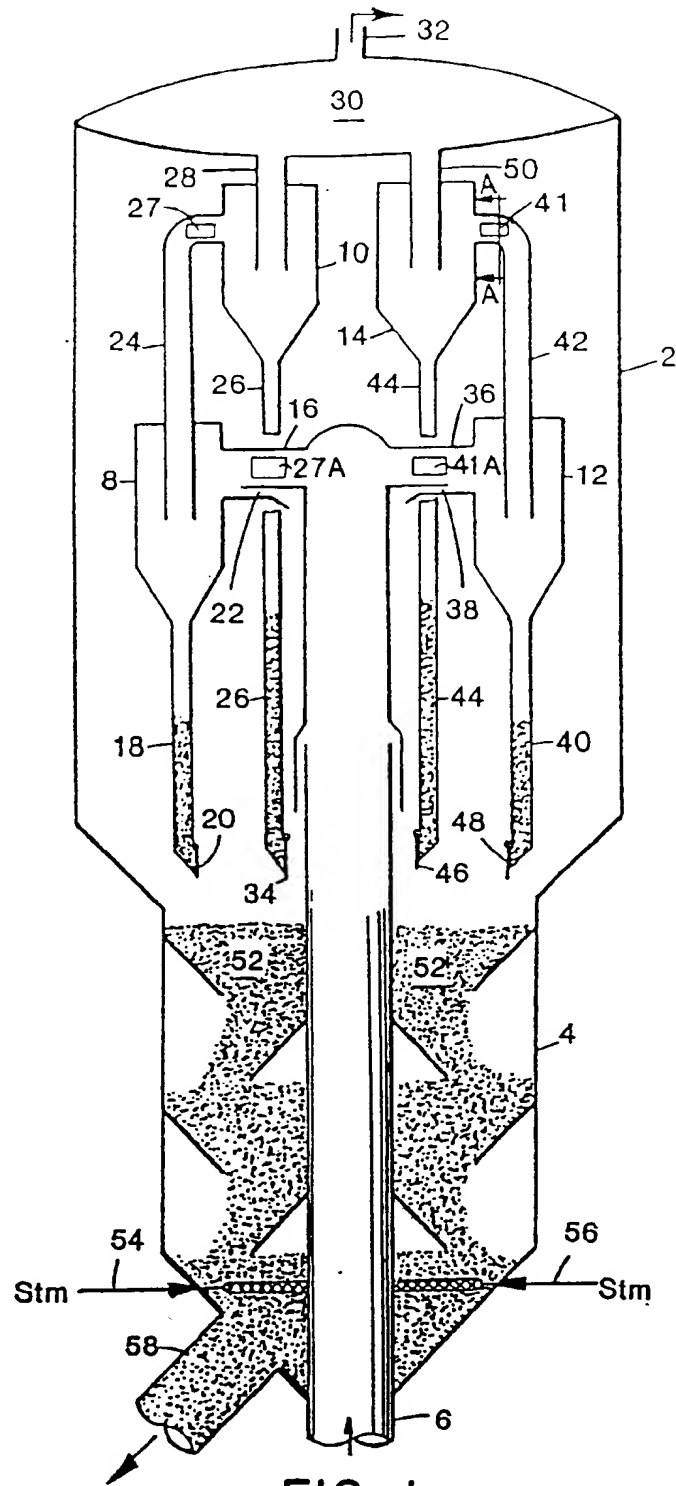


FIG. 1

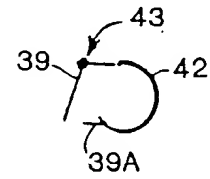


FIG. 2